

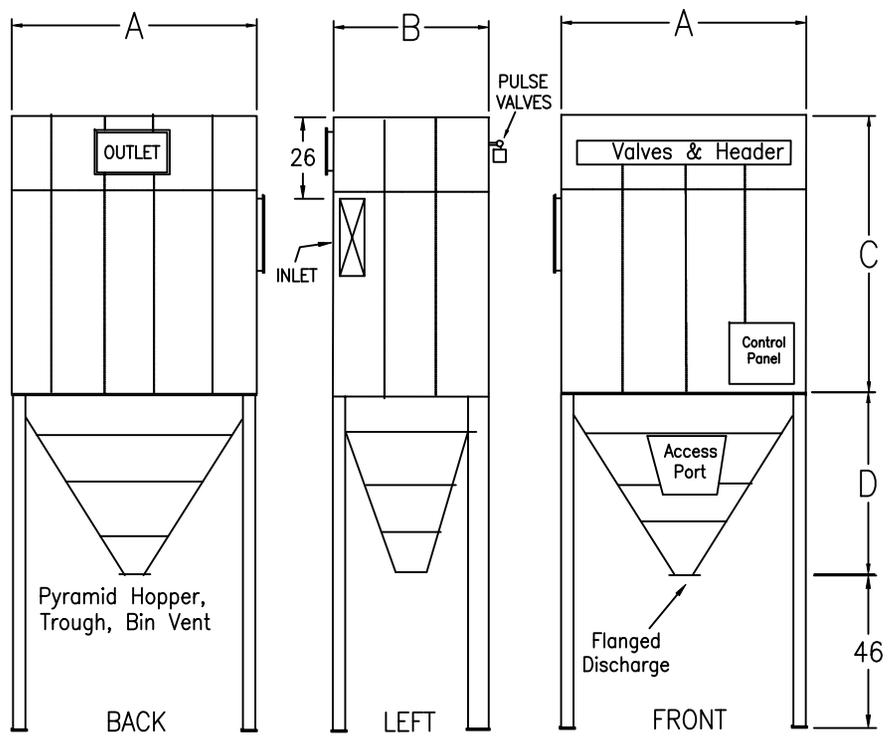
Model	Rated Volume (CFM)	Filter Area (ft ²)	Qty bags/Length	Compressed Air Consumption (SCFM) (1)	Hopper	Hopper Discharge	Inlet	Outlet	A	B	C	D	Weight (lbs)	Model
SINGLE WIDTH - 5 FOOT BAG														
36VS-5	5,700	311	36/66	1.12-2.24	pyramid	10x10	26x12	26x12	60	72	90	56	2350	36VS-5
48VS-5	7,500	415	48/66	1.49-2.98	pyramid	10x10	36x12	36x12	78	72	90	55	2625	48VS-5
60VS-5	9,500	519	60/66	1.86-3.72	Pyramid	10x10	40x14	40x14	98	72	90	75	3200	60VS-5
SINGLE WIDTH - 8 FOOT BAG														
36VS-8	8,600	453	36/96	1.80-1.60	pyramid	10x10	35x14	35x14	60	72	120	56	2700	36VS-8
48VS-8	11,500	603	48/96	2.40-4.80	pyramid	10x10	48x14	40x16	78	72	120	55	3400	48VS-8
60VS-8	14,500	754	60/96	3.00-6.00	Pyramid	12x12	60x14	45x18	98	72	120	75	4300	60VS-8
72VS-8	17,200	905	72/96	3.60-7.20	(2)	(2)10x10	76x14	54x18	120	72	120	56	4900	72VS-8
84VS-8	20,000	1056	84/96	4.20-8.40	(2)	(2)10x10	78x16	66x18	135	72	120	56	6750	84VS-8
96VS-8	23,000	1207	96/96	4.80-9.60	(2)	(2)10x10	90x16	78x18	154	72	120	60	7650	96VS-8

Selecting a collector based on Fitler ratio is an engineering mistake. See Engineering Bulletin, E-002.

Operating Requirements:
 For best cleaning, both the process air and compressed air must be maintained at least 15oF above the dew point. Compressed air must be below a maximum temperature of 180°F at 85 PSI. For the protection of the pneumatic valves and controls, compressed air for this equipment must be clean and have a refrigerant or desiccant dryer at the collector having a low enough dew point to meet conditions of operation

All Dimensions in Inches

- (1) dust loading of 2-8 grains per cu. ft.
- (2) two pyramid hoppers



- 12 gauge hot rolled steel, fully welded construction, strategically placed vertical re-inforcing bars to withstand +/-20"wc,
- High side inlet with large dropout chamber, perforated baffle, to prevent abrasion and distribute air/dust evenly on filters. Downward flow prevents upward "can velocity".
- 60°Pyramidal hoppers or troughs provided for dust collection.
- SSPC-SP3 power-tool cleaned, epoxy primed (in and out) and exterior finish coat of Terra Brown (RAL8028) paint, good to 250°F.
- Automatic self-cleaning, advanced technology "high-ratio" reverse jet pulse, requiring no shutdown for after-pulse cleaning. Pulse sequencer supplied in NEMA 4 enclosure.
- Diaphragm valves rated at 125% of required flow to ensure proper back-flush volume.
- Computer designed supersonic converging-diverging nozzles on pulse pipes.
- One differential pressure gauge and dust trap with connecting hardware.
- One full set of top-removal filter bags and wire cages.
- Built to North American compliance with EPA, OSHA NFPA standards. Compliance with local codes and standards are the responsibility of the purchaser.

QAM reserves the right to change design and specifications without notice.

Manufactured to:



COMPANY:			QUALITY AIR MANAGEMENT		
TITLE:			VS-Series Baghouse Dust Collector		
DWG.No.	V-001		REV. No.	2	
DATE:	9/13/2017		DATE:	5/1/2018	
SCALE:			NOT TO SCALE		
DRAWN BY:			GRB		

MODEL	Rated Volume (scfm)	Filter Area (ft²)	# OF BAGS/ LENGTH	Compressed Air Consumption (3) (scfm)	Hopper	INLET H x W	OUTLET diameter	A	B	C	D	E	Weight (lbs)	MODEL
DOUBLE WIDTH - 8 FOOT BAG														
120VD-8	29,000	1508	120/96	6.00 - 12.00	(1)	50x30	40	97	160	103	96	75	8100	120VD-8
144VD-8	35,000	1810	144/96	7.20 - 14.40	(1)	54x30	44	113	160	103	96	87	9200	144VD-8
168VD-8	40,000	2112	168/96	8.40 - 16.80	(1)	64x30	48	113	179	103	96	87	10,300	168VD-8
192VD-8	46,000	2413	192/96	9.60 - 19.20	(1)	72x30	48	113	198	103	96	87	11,100	192VD-8
DOUBLE WIDTH - 10 FOOT BAG														
168VD-10	58,000	2640	168/120	11.76 - 23.52	(1)	54x48	54	113	197	127	120	87	12,200	168VD-10
192VD-10	67,000	3017	192/120	13.44 - 26.88	(1)	60x48	60	113	216	127	120	87	13,100	192VD-10
216VD-10	75,000	3394	216/120	15.12 - 30.24	(2)	72x48	60	113	235	127	120	90	13,900	216VD-10
240VD-10	83,000	3770	240/120	16.80 - 33.60	(2)	80x48	66	113	254	127	120	87	15,800	240VD-10
264VD-10	91,000	4148	264/120	18.48 - 36.96	(2)	84x48	72	113	273	127	120	87	16,900	264VD-10
288VD-10	100,000	4525	288/120	20.16 - 40.32	(2)	90x48	76	113	292	127	120	87	17,900	288VD-10

Selecting a collector based on Filtler ratio is an engineering mistake. See Engineering Bulletin, E-002.

Operating Requirements:

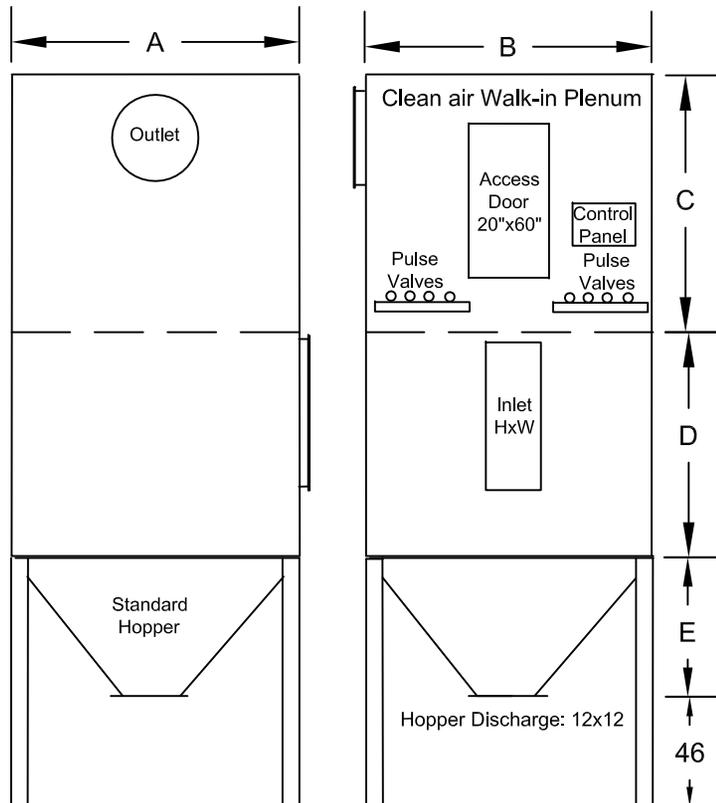
For best cleaning, both the process air and compressed air must be maintained at least 15°F above the dew point. Compressed air must be below a maximum temperature of 180°F at 85 PSI. For the protection of the pneumatic valves and controls, compressed air for this equipment must be clean and have a refrigerant or desiccant dryer at the collector having a low enough dew point to meet conditions of operation.

- (1) 2 pyramid hoppers
- (2) 3 pyramid hoppers
- (3) compressed air used for a dust loading of 2-8 grains per cu.ft.

All Dimensions in inches

- 12 gauge hot rolled steel, fully welded construction, strategically placed vertical re-inforcing bars to withstand +/-20"wc,
- High central inlet with large dropout chamber, perforated baffle, to prevent abrasion and distribute air/dust evenly on filters. Downward flow prevents upward "can velocity".
- 60°Pyramidal hoppers or troughs provided for dust collection.
- SSPC-SP3 power-tool cleaned, epoxy primed and exterior finish coat of Terra Brown (RAL8028) paint, good to 250°F.
- Automatic self-cleaning, advanced technology "high-ratio" reverse jet pulse, requiring no shutdown for after-pulse cleaning. Pulse sequencer supplied in NEMA 4 enclosure.
- Diaphragm valves rated at 125% of required flow to ensure proper back-flush volume.
- Top-removal bags allows quick and easy inspection and servicing without precarious position for the operating personnel.
- Computer designed supersonic converging-diverging nozzles on pulse pipes.
- One differential pressure gauge and dust trap with connecting hardware.
- One full set of top-removal filter bags and wire cages.
- Built to North American compliance with EPA, OSHA NFPA standards. Compliance with local codes and standards are the responsibility of the purchaser.

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Manufactured to:



COMPANY:		
QUALITY AIR MANAGEMENT		
TITLE:		
VD-Series Baghouse Dust Collector		
DWG.No.	V-002	REV. No.
DATE:	9/28/2017	SCALE:
	NOT TO SCALE	DRAWN BY:
		GRB

(as a governing specification in cylindrical bag pulse jet dust collectors)

The History of Reverse Jet and Pulse Jet Design and Development must be reviewed to determine proper selection of collectors.

The first pulse jet collector was developed by Pulverizing Machinery of Summit New Jersey in the early 60's, to collect dust from their Pulverizers. They had tried to use the Blow-ring design but they could not handle the dust (powder) loads as their grinder Pulverizers became bigger. The typical load to the collectors from the Pulverizers were between 150 and 300 grains per cubic foot. The collector design was based on the same blow-ring filtering velocities at these loads. The cages were based on available designs from shipping pulverizer shafts. The pulse valves selected were diaphragm valves that were the fastest and the lowest cost valve available. This valve happened to be a ¾ inch diaphragm pilot operated valve. They decided to use several valves in a collector and pulse them with an electronic timer. It was found the hole sizes and venturi formed an air ejector design that had the same jet velocity that the blow-ring collector was using. But the big breakthrough came with the realization that the dust was ejected from the bag during the first 4 or 5 milliseconds of the valve opening. The valves were operated as fast as the mechanical design allowed. The operation was completed in less than 0.10 seconds. It became apparent that the frequency of cleaning was a function of the load to the collector. For instance, for loadings of 300 grains, the collectors would operate at a filtering velocity of between 7 and 9 ft per minute. At material handling facilities such as quarries, the collector would run at velocities of 14 to 16 feet per minute. The typical pressure drop in these collector designs were about 3.5 inches WC pressure for the high loads and 2.0 inches WC for the lower dust loads. The typical compressed air usage, on the high loads, was 1 to 2 SCFM per 1000 CFM of filtered air. For loads under 10 grains per cubic foot, the air usage was 0.2 to 0.8 SCFM per 1000 CFM of filtered air.

Determining the filter velocity (then referred to as filter ratio) became a rather complicated procedure. The ratio presumably was determined by dust load, fineness of the dust, temperature of process gas stream, and other factors.

The hopper inlet was a carry over design from both the blow-ring collector and the previous mechanical shaker collectors.

By 1969, there were over 10,000 collectors in operation. Almost all of them were installed on process exhaust from Pulverizers or in foundries. Pulverizing Machinery changed their name to Mikropul and licensed FlexKleen to also build and Market collectors. The collectors for MikroPul had 4 ½ inch diameter bags 72 inch long and the FlexKleen units had 5 inch bags 102 inches long. Bag life was 3-5 years on Pulverizer applications and over eight years on low loading applications.

Engineering Disaster 1971

In 1971, the patent was challenged and the Pulverizing Machinery patent was declared invalid. The market changed radically because Air Pollution Control Regulations also became effective at the same time. Many new suppliers entered the market. In order to compete, Mikropul changed their design. They went from 6 foot to 10 foot bags. They increased their pulse pipe holes by the same ratio. The whole industry followed and copied the new design for hole size and venturi throat diameter. At the time, Mikropul had 40,000 ventures in stock and kept the same venturi sizes. This increased the jet velocity of the cleaning jet by 66 per cent.

This was when the dust collector market was growing at a 20% annual rate. With the new designs:

- (1) pressure drop increased to 4 ½ to 6 ½ inches WC
- (2) Compressed air consumption increased by over 50% for similar applications.
- (3) Bag life was reduced by over 50%.
- (4) In reaction to these problems the filter ratios were reduced to between 4 & 6 on almost all applications.

Reasons for Disaster

What happened was no one at that time realized what might have been a rather obvious truth, that the velocity with which the dust is ejected from the bag during cleaning is proportional to the velocity of the cleaning jet. At the new velocities, dust is driven toward adjacent rows of bags in the filter mode. Depending on the dust density, the dust will be driven through the adjoining cake into the clean side of the bags. The cake becomes more dense and the pressure drop increases until the process stabilizes which takes 16-100 hours. Even after the equilibrium, the dust still penetrates and bag wear is high. With low filter ratios it takes longer for the bag to wear out and require longer times between replacements.

Today's Conditions

This disastrous design continues to be employed by most of the pulse jet collector suppliers in the world.

New Advanced Technology eliminates design flaws; allows for High Ratio Operation

In 1981 a new technology was developed, a pulse jet collector that basically changed the cleaning system design. The key to this design was to change the jet velocity to a fraction of the existing designs. New Technology eliminated the penetration of dusts from the row of cleaning bags to the adjoining row in a filtering mode.

This allowed pulse jet collectors to operate at:

- (1) lower pressure drops (1 - 3 inches WC),
- (2) lower compressed air consumption for cleaning (50 - 75% less)
- (3) 3 to 4 times longer bag life
- (4) filter ratios of over 14:1 on any application
- (5) decrease dust penetration by up to 90%.

There have been several suppliers building and selling these New Technology collectors since 1982. In fact the patents have now expired. **There are over 4000 installations worldwide.**

Why is this New Technology not accepted by all the major suppliers?

- 1) If you produced 40,000 collectors after the development of the new technology was published over 20 years ago, you might be subject to legal action for poor judgment and causing the public to be overcharged for their dust collection.
- 2) They do not have the engineering expertise to build these new technology collectors.
- 3) People using the old obsolete technology control over 90% of the market world-wide.
- 4) The suppliers of valves and filter elements would have their markets cut in half.
- 5) Air compressor sales and service for pulse jet collectors would be cut by 60%

Modifying existing collectors with almost no risk to the purchaser.

We can supply new bags, pulse pipes and bag plugs to alter performance to high technology low pressure drop, reduced air consumption, lower penetration (immediately noticeable) and long bag life (it takes some time to verify that but it should be obvious from the other indications). The modifications take only a few hours and if a customer is not satisfied, he can return pipes and cages for credit and re-install the old components. **If this was not an absolute certainty customers would not pay for the equipment.**