

MODEL	Rated Volume (CFM)	Filter Area (SFT)	Qty Bags Length(in)	Compressed Air (SCFM)	Inlet	Std Outlet	Dust Drawer (cu.ft.)	A	B	C	D	E	F	Weight (lbs)	MODEL
6LC-H	500	29	6/48	0.19	5" dia.	5" dia.	-	21	21	71	28	18	19	483	6LC-H
6LC-L	500	29	6/48	0.19	5" dia.	5" dia.	2.5	21	21	76	-	18	19	483	6LC-L
9LC-H	720	43	9/48	0.28	6" dia	6" dia	-	27	27	76	28	18	19	554	9LC-H
9LC-L	720	43	9/48	0.28	6" dia	6" dia	3	27	27	76	-	18	19	554	9LC-L
12LC-H	960	57	12/48	0.37	7" dia	7" dia	-	27	27	76	47	18	22	778	12LC-H
12LC-L	960	57	12/48	0.37	7" dia	7" dia	4	27	27	76	-	18	22	778	12LC-L
18LC-H	1440	85	18/48	0.56	12x6"	12x6"	-	27	27	86	47	18	26	1093	18LC-H
18LC-L	1440	85	18/48	0.56	12x6"	12x6"	6	27	27	76	-	18	26	1093	18LC-L
30LC-H	2400	142	30/48	0.94	18x6"	18x6"	-	39	39	86	47	18	29	1880	30LC-H
30LC-L	2400	142	30/48	0.94	18x6"	18x6"	8.5	39	39	76	-	18	29	1880	30LC-L
30LC8-H	4800	283	30/96	2.55	35x8"	35x8"	-	39	39	143	47	22	35	2679	30LC8-H
30LC8-L	4800	283	30/96	2.55	35x8"	35x8"	8.5	39	39	127	-	22	35	2679	30LC8-L

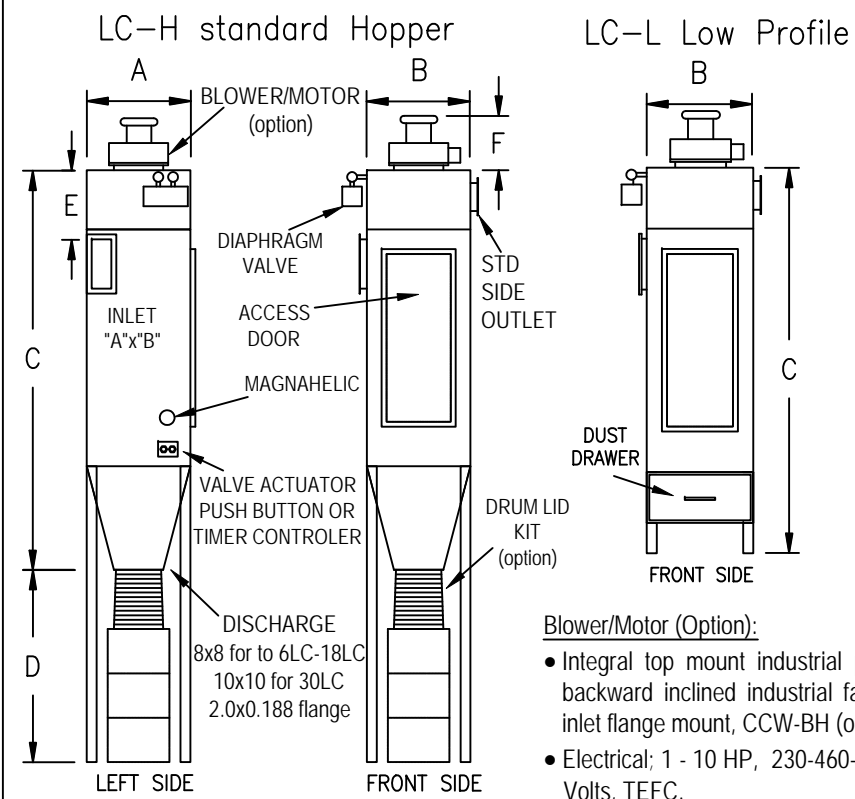
FAN PERFORMANCE	CFM @ In. WC, external pressure					Motor HP	Noise, dBA(1)	Weight (lbs)
	0	1	2	4	6			
6LC	620	590	545	460	320	1	74	57
9LC	820	790	750	660	550	2	78	96
12LC	1100	1050	970	810	660	3	77	137
18LC	1575	1500	1440	1300	1150	5	84	183
30LC	2775	2600	2500	2200	1775	5	80	215
30LC8	5400	5100	4900	4500	4150	10	87	371

High-static blowers also available

(1) Noise level is rated at 5 feet from fan outlet, position 1. The environment for each fan installation influences its measured sound value, therefore dBA levels cannot be guaranteed.

Hopper and Stand; 6LC-H & 9LC-H sized for 5 gallon pail, 12LC-H to 30LC8-H sized for 45 gallon drum.

All dimensions in inches



- 12 gauge hot-rolled steel welded construction, to withstand +/- 20" WG,
- High inlet leads to large drop out section where the air makes a 90deg turn into the filter section. This prevents abrasion and forces most of the dust to drop directly to the collection hopper, no "can" velocity issues..
- 60° Pyramidal hopper provided for dust collection. Optional drum lid adapter available, **drum supplied by others.**
- Large access door to bag filter compartment with easy to open/close hand knobs.
- Inlet/outlet; round collar for slip connection, or, flanged rectangular.
- SSPC-SP3 power-tool cleaned, epoxy primed and exterior finish coat of Terra Brown (RAL8028) paint, good to 250°F
- Automatic self-cleaning, advanced technology "high-ratio" reverse jet pulse, requiring no shutdown for after-pulse cleaning. Pulse sequencer supplied in NEMA 4 enclosure. No need to shutdown the collector during a cleaning cycle.
- Diaphragm valves rated at 125% of required flow to ensure proper back-flush volume.
- One differential pressure gauge with connecting hardware.
- One full set of bottom removal filter bags and wire cages.
- Built to North American compliance with EPA, OSHA NFPA standards. Compliance with local codes and standards are the responsibility of the purchaser.

Operating Requirements:

For best cleaning, both the process air and compressed air must be maintained at least 15°F above the dew point. Compressed air must be below a maximum temperature of 180°F at 85 psig. For the protection of the pneumatic valves and controls, compressed air for this equipment must be clean and have a refrigerant or desiccant dryer at the collector having a low enough dew point to meet conditions of operation.

Blower/Motor (Option):

- Integral top mount industrial pressure blowers, or, backward inclined industrial fans, arrangement 4V, inlet flange mount, CCW-BH (outlet to the right side).
- Electrical; 1 - 10 HP, 230-460-575 / 3 phase / 60 Hz Volts, TEFC.

Selecting a collector based on Filtler ratio is an engineering mistake. See Engineering Bulletin, E-002.

Manufactured to



Quality Air Management reserves the right to change design and specifications without notice.

DRAWINGS BY: Dave Palladini DLP Drafting 519-841-9500 dpalla1077@rogers.com	COMPANY: QUALITY AIR MANAGEMENT Phone: 1-800-267-5585 www.qamanage.com	ALL DIMENSIONS ARE IN INCHES UNLESS STATED OTHERWISE	PROJECTION:		
			TITLE: "LC" series Small Baghouse Dust Collector	PAGE: 1 of 1	DATE: 9/22/2017
		1 9/17/18 Add PISG designation	REVISION DESCRIPTION.		
		REV. No. REV. DATE.			

(as a governing specification in cylindrical bag pulse jet dust collectors)

The History of Reverse Jet and Pulse Jet Design and Development must be reviewed to determine proper selection of collectors.

The first pulse jet collector was developed by Pulverizing Machinery of Summit New Jersey in the early 60's, to collect dust from their Pulverizers. They had tried to use the Blow-ring design but they could not handle the dust (powder) loads as their grinder Pulverizers became bigger. The typical load to the collectors from the Pulverizers were between 150 and 300 grains per cubic foot. The collector design was based on the same blow-ring filtering velocities at these loads. The cages were based on available designs from shipping pulverizer shafts. The pulse valves selected were diaphragm valves that were the fastest and the lowest cost valve available. This valve happened to be a ¾ inch diaphragm pilot operated valve. They decided to use several valves in a collector and pulse them with an electronic timer. It was found the hole sizes and venturi formed an air ejector design that had the same jet velocity that the blow-ring collector was using. But the big breakthrough came with the realization that the dust was ejected from the bag during the first 4 or 5 milliseconds of the valve opening. The valves were operated as fast as the mechanical design allowed. The operation was completed in less than 0.10 seconds. It became apparent that the frequency of cleaning was a function of the load to the collector. For instance, for loadings of 300 grains, the collectors would operate at a filtering velocity of between 7 and 9 ft per minute. At material handling facilities such as quarries, the collector would run at velocities of 14 to 16 feet per minute. The typical pressure drop in these collector designs were about 3.5 inches WC pressure for the high loads and 2.0 inches WC for the lower dust loads. The typical compressed air usage, on the high loads, was 1 to 2 SCFM per 1000 CFM of filtered air. For loads under 10 grains per cubic foot, the air usage was 0.2 to 0.8 SCFM per 1000 CFM of filtered air.

Determining the filter velocity (then referred to as filter ratio) became a rather complicated procedure. The ratio presumably was determined by dust load, fineness of the dust, temperature of process gas stream, and other factors.

The hopper inlet was a carry over design from both the blow-ring collector and the previous mechanical shaker collectors.

By 1969, there were over 10,000 collectors in operation. Almost all of them were installed on process exhaust from Pulverizers or in foundries. Pulverizing Machinery changed their name to Mikropul and licensed FlexKleen to also build and Market collectors. The collectors for MikroPul had 4 ½ inch diameter bags 72 inch long and the FlexKleen units had 5 inch bags 102 inches long. Bag life was 3-5 years on Pulverizer applications and over eight years on low loading applications.

Engineering Disaster 1971

In 1971, the patent was challenged and the Pulverizing Machinery patent was declared invalid. The market changed radically because Air Pollution Control Regulations also became effective at the same time. Many new suppliers entered the market. In order to compete, Mikropul changed their design. They went from 6 foot to 10 foot bags. They increased their pulse pipe holes by the same ratio. The whole industry followed and copied the new design for hole size and venturi throat diameter. At the time, Mikropul had 40,000 ventures in stock and kept the same venturi sizes. This increased the jet velocity of the cleaning jet by 66 per cent.

This was when the dust collector market was growing at a 20% annual rate. With the new designs:

- (1) pressure drop increased to 4 ½ to 6 ½ inches WC
- (2) Compressed air consumption increased by over 50% for similar applications.
- (3) Bag life was reduced by over 50%.
- (4) In reaction to these problems the filter ratios were reduced to between 4 & 6 on almost all applications.

Reasons for Disaster

What happened was no one at that time realized what might have been a rather obvious truth, that the velocity with which the dust is ejected from the bag during cleaning is proportional to the velocity of the cleaning jet. At the new velocities, dust is driven toward adjacent rows of bags in the filter mode. Depending on the dust density, the dust will be driven through the adjoining cake into the clean side of the bags. The cake becomes more dense and the pressure drop increases until the process stabilizes which takes 16-100 hours. Even after the equilibrium, the dust still penetrates and bag wear is high. With low filter ratios it takes longer for the bag to wear out and require longer times between replacements.

Today's Conditions

This disastrous design continues to be employed by most of the pulse jet collector suppliers in the world.

New Advanced Technology eliminates design flaws; allows for High Ratio Operation

In 1981 a new technology was developed, a pulse jet collector that basically changed the cleaning system design. The key to this design was to change the jet velocity to a fraction of the existing designs. New Technology eliminated the penetration of dusts from the row of cleaning bags to the adjoining row in a filtering mode.

This allowed pulse jet collectors to operate at:

- (1) lower pressure drops (1 - 3 inches WC),
- (2) lower compressed air consumption for cleaning (50 - 75% less)
- (3) 3 to 4 times longer bag life
- (4) filter ratios of over 14:1 on any application
- (5) decrease dust penetration by up to 90%.

There have been several suppliers building and selling these New Technology collectors since 1982. In fact the patents have now expired. **There are over 4000 installations worldwide.**

Why is this New Technology not accepted by all the major suppliers?

- 1) If you produced 40,000 collectors after the development of the new technology was published over 20 years ago, you might be subject to legal action for poor judgment and causing the public to be overcharged for their dust collection.
- 2) They do not have the engineering expertise to build these new technology collectors.
- 3) People using the old obsolete technology control over 90% of the market world-wide.
- 4) The suppliers of valves and filter elements would have their markets cut in half.
- 5) Air compressor sales and service for pulse jet collectors would be cut by 60%

Modifying existing collectors with almost no risk to the purchaser.

We can supply new bags, pulse pipes and bag plugs to alter performance to high technology low pressure drop, reduced air consumption, lower penetration (immediately noticeable) and long bag life (it takes some time to verify that but it should be obvious from the other indications). The modifications take only a few hours and if a customer is not satisfied, he can return pipes and cages for credit and re-install the old components. **If this was not an absolute certainty customers would not pay for the equipment.**